



REVIEW OF EMERGING NUTRIENT RECOVERY TECHNOLOGIES AND DISCUSSION ON PERFORMANCE/COST STRUCTURES FOR WSU/DVO INTEGRATED APPROACH

Capturing Valuable Nutrients from Manure: Part 2

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Outline

- Role of Anaerobic Digestion, Organic Waste, Co-Digestion and Wastewater Application/Treatment
- Phosphorus Treatment Options
- Nitrogen Treatment Options
- Combined Treatment Options/Capabilities
- WSU DVO System
- Partitioning Example
- Considerations for Federal/State Government and Project Developers

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Anaerobic Digestion



- Remove 90% of odors¹.
- Destroy 99% or >2.0 log of indicator pathogens in manure².
- Reduce GHG emissions by 3-4 MT CO_{2eq}/cow year compared to baseline².
- Produce renewable energy at a rate of 0.25 KW/cow/yr or 167 DGE/cow/yr².
- Stabilize volatiles, reduce solids, separate fiber, shift nutrients towards inorganic form².

¹ Wilkie 2000 ² Frear et al., 2011

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Organic Waste



- 26-40% of all US food wasted—2% of US energy consumption embedded in this loss¹.
- Diverted use (no landfilling) leads to doubling of economic benefit to state, 1/5 reduction in treatment costs, and significant reductions in odor, GHG, and VOC^{2,3}.
- Waste organics represent significant recovered energy potential—2 to 4x that of dairy manure.

¹ Kantor and Lipton (1997); ² Goldman and Ogishi, 2001; Bloom 2010; ³ Mata-Alvarez et al., 2000; Bernstad et al., 2011

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Manure Wastewater



- Each cow annually excretes 60 and 7 kg of N and P, respectively¹
- Trend towards larger CAFOs which apply at a rate 3x that of smaller farms. Only 23% and 1% of large CAFOs applying manure at agronomic rates for N, P respectively^{2,3,4}
- Impacted soils lead to concerns in N/P eutrophication, nitrate-induced conditions, PM-2.5, ammonia health, GHG release, yield loss, etc.

¹ ASAE 2005; ² USDA NASS, 2010; ³ Macdonald and McBride 2009; ⁴ Ribeyro et al., 2003

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Case Study and Expansion

While co-digestion business model is developed, albeit under electrical pricing pressure, new NR unit installations can add eco-system benefits while still supplying total system economic viability.

A Business Model for Sustainable Dairy Digester Systems

- Crop Fertilizer:** \$100,000 annual revenue (100,000 annual avoided cost)
- Renewable Energy:** 5 million kWh to power nearby 100 houses; \$400,000 annual revenue; Renewable Energy Credits (RECs) 5 million RECs; \$100,000 annual revenue
- Carbon Offsets:** 11,000 tons CO₂ offset; \$100,000 annual revenue
- Surface water:** Create new revenue via energy; Advance sustainable products
- Manure:** 4,000 lactating dairy cows; 100,000 cubic yards of digester floor; \$100,000 annual revenue
- Rich Dairy Soil Amendment:** 10,000 cubic yards of digester floor; \$100,000 annual revenue
- Local Retailer:** 100,000 cubic yards of digester floor; \$100,000 annual revenue
- Other Revenue:** 100,000 annual avoided cost; 100,000 annual avoided cost; 100,000 annual avoided cost

Revenue Items

- CHP/CNG
- Fiber/Peat
- Carbon Offset
- RIN/RECs
- Tipping Fee
- Renewable Fertilizers
- Farm Manure Mgmt. Savings

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Phosphorus Treatment

Nearly 80% of digested dairy manure phosphorus is in the form of suspended fine solids¹—lending at least some of P removal to a mechanical approach.

Industry Mainstay
Primary and Secondary Screening

- Various forms and sequence of screens allows for separation of desired fibrous solids (8-10 yards/cow/year) as well as secondary non-fibrous solids.
- 15-30% recovery of phosphorus and nitrogen from liquid stream.
- \$5-6/cow/year—O/M costs, \$32-36/cow—Capital costs.
- Fiber product has 70% moisture—\$5-15/yard revenue.

¹ Gungor and Karthikeyan, 2008; Pastor et al., 2010

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Phosphorus Treatment

Given the degree of P-impacted soils near/around dairy CAFOs, important to achieve at least 75-80% recovery of phosphorus.

Next Generation Available

Solids/Polymer Coagulation

- **80-90%** recovery of phosphorus and **35-55%** nitrogen from liquid.
- **\$25-75/cow/year**—O/M costs, **\$120-150/cow**—Capital costs.
- Cost affected by amount/type polymer/coagulant.
- Drying, organic cert. are concern.



Struvite Crystallization

- **75%** recovery of phosphorus and **30%** nitrogen from liquid.
- **\$90-110/cow/year**—O/M costs, **\$100-150/cow**—Capital costs.
- Nice crystal product.
- Effective NPK formulation.
- Limited drying and modifying.
- No organic cert.



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Phosphorus Treatment

While other approaches with intriguing possibilities and their own set of concerns do exist, analysis demonstrates that **polymer/coagulation** and **struvite crystallization** technologies (in conjunction with fibrous screening) appear to offer the most viable approaches to maximum, primary P removal.

Note that costs/concerns do still exist and markets need to be developed and Project Developers as well as agencies should be aware of capital and O/M costs to accomplish such recovery.

Key Technology	Performance	Operating Cost	Capital Cost	Scale
Primarily P		/cow/year	/cow	
1' and 2' Mechanical Screens	TN 15-30%, P 15-25%	\$5-6	\$32-36	Commercial
Centrifuge-No Polymer/Coagulant	TN 24-30%, TP 50-65%	\$25-50	\$57-136	Commercial
Lime Precipitation	TN 30-40%, TP 70-80%	\$30-60	\$60-80	Pilot
Mechanical + Polymer/DAF	TN 45-55%, TP 85-90%	\$25-30	\$130-150	Commercial
Mechanical + Polymer Belt Press	TN 35-45%, TP 75-85%	\$50-75	\$120-140	Commercial
Struvite Crystallization	TN 30%, TP 75%	\$90-110	\$100-150	Commercial
Mechanical + Electrocoagulation	TN 30-50%, TP 80-90%	\$140-160	\$200-225	Pilot
Mechanical Screening + Membrane	TN 71-73%, TP 80-90%	\$125-150	\$275-330	Pilot
Enhanced Biological Phosphorus	TP 42-91%	\$150-170	\$275-300	Pilot

Table not intended to be complete evaluation of all technologies or companies, nor are cost estimates final, and are only approximate

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Nitrogen Treatment

Ammonia/Organic N ratio is roughly 1:1 and 2:1 in non-digested and digested dairy manure, respectively. Being soluble, ammonia-N more difficult and costly to recover at large percentages.

- **Organic N Recovery via Screens/Polymer Coagulation**
 - **35-55% TN recovery** at \$25-75 O/M and \$120-150 Capital
 - Simultaneous recovery of P
- **Ammonia Recovery (Various Stripping or Membranes)**
 - **40-70% TN recovery** at \$80-160 O/M and \$375-550 Capital
 - Saleable ammonium salt product, solution or crystals
- **Partial Nitrification/De-nitrification**
 - **80-90% TN loss** at \$60-80 O/M and \$300-400 Capital
 - Long retention time, loss to N₂
- **Nitrification/De-nitrification**
 - **80-90% TN loss** at \$80-100 O/M and \$300-400 Capital
 - Scale and size issues, carbon input costs, loss to N₂

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Nitrogen Treatment

Notable extra cost to reduce/recover N with considerations needed in regard to recovering N or blowing it off as N₂. Decision tied to complexity of producing, storing, blending, and marketing N-product.





Key Technology	Performance	Operating Cost /cow/year	Capital Cost /cow	Scale
Primarily N				
Flash Distillation of Ammonia	TN 60-70%	\$80-120	\$475-550	Pilot
Chemical Ammonia Stripping	TN 50-60%	\$120-160	\$375-425	Pilot
Non-Chemical Ammonia Stripping	TN 40-60%	\$80-120	\$375-425	Commercial
Nitrification/Denitrification	TN 80-90%	\$80-100	\$300-400	Pilot
Partial Nitrification/Denitrification	TN 80-90%	\$60-80	\$300-400	Lab
Gas-Permeable Membranes	TN 60-70%	NA	NA	Lab

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Combined Treatments

- As many farms are under greater pressure for P management and the cost of N recovery is comparatively more costly, it makes sense to use P only recovery technologies for these P management situations.
- In regard to those under N management concerns, because of cost, it makes sense to utilize combined technologies that remove high percentages of both N and P.
- While the focus of this presentation is mostly AD followed by nutrient recovery technology, it is very important to note that alternative renewable energy systems such as combustion/pyrolysis/gasification can also recover nutrients, including potassium (K).
- Algae as a bio-treatment within an algal fuel bio-refinery is an active concept.

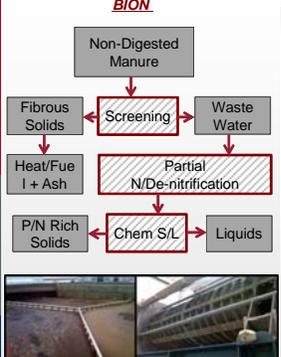


Algeolve, 2013

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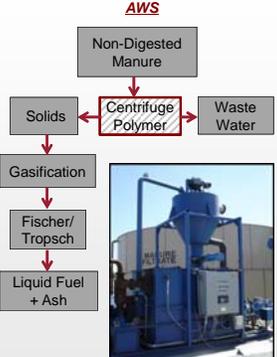
Non-AD Based Examples

BION



BION System, 2011

AWS

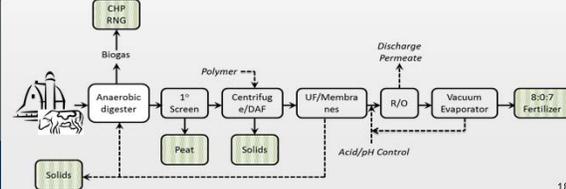


Agricultural Waste Solutions (AWS), 2010

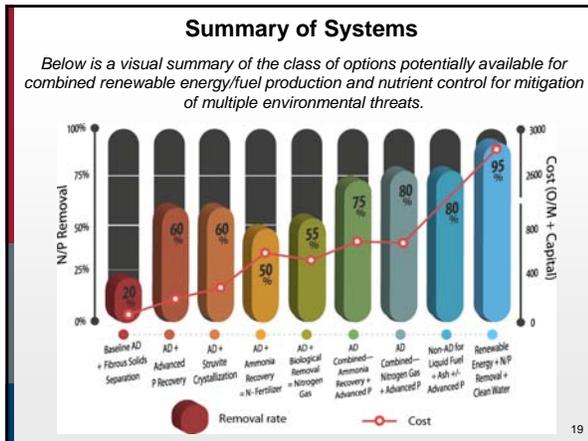
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Salt Removal/Clean Water

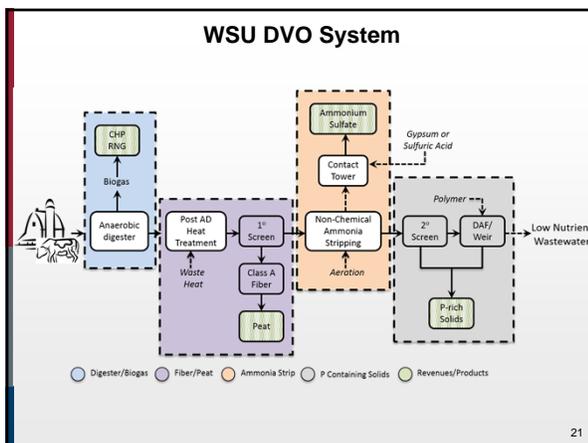
- Removal of salts and movement towards production/utilization of clean water is at another level of complexity and cost.
- Using many of the already described, sequential steps, it is then possible to use additional operations involving membranes and reverse osmosis to produce both a near complete clean water AND concentrated nutrient/salt rich fertilizers.
- While potentially organically certifiable fertilizers as well as response to salt concerns can be realized, energy/input costs are high and on the order of \$2,000-3,000 combined capital/OM costs



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Tech Choice—Considerations

- *Concept/Pilot vs. Commercially Available.* No substitutes for practical and scaled experience. Numerous lessons, strongly affecting cost, performance and viability are learned during scale up.
- *Sequential vs. Direct Treatment.* Heterogeneous waste with high solids and nutrient content often requires sequential treatment, lending an ear towards sequential removal of contaminants as opposed to more direct means.
- *Operating vs. Capital.* If appropriate and viable technologies are chosen, then capital is a one-time cost, which of course is preferably made low, but operating is an annual cost that can continually bring a project in the red. Caution for high electrical and chemical costs.
- *Product Sales.* Renewable fertilizer/amendment markets either don't exist or are immature. Caution in regard to price points and volume as well as hidden costs in storage, transportation, blending, quality of product, etc.

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Regulator—Considerations

- Requirement of BACT nutrient technologies do have costs associated with them and as a result any policy decisions must take into consideration *how and to whom these costs will be accommodated.*
- *A systems viewpoint is preferred, renewable energy production can be the economic and conversion facilitator* for nutrient recovery, but only if the economic margin gained by the energy production can incur the costs. Thus renewable energy policy decisions are key:
 - *CNG*—RIN value and category confidence, LCF standards, carbon markets, CNG engine certification, pipeline access/tariff standardization, infrastructure incentives, etc.
 - *CHP*—Elevated Renewable Energy Portfolios, carbon markets, alleviation of natural-gas linked deferred cost tables, etc.
- *White Elephants:* Beware nutrient markets producing 'white elephant' projects with high cost—best to have projects held to what market can demand with 'some' well conceived policy assistance.

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Regulator—Considerations

- *Nutrient Markets*—Generating new markets and competing against fossil fertilizer is complex, time-consuming and fraught with uncertainty. Policy could potentially leverage or spur the market to assist in its development.
- *Financing*—While renewable energy projects might receive external financing, non-proven nutrient recovery components perhaps required as a 'cost of doing business' are at best difficult to finance. Federal programs aimed at 'extra-value' funding would be useful.
- *Federal Center of Excellence*—Numerous additional technical needs are required for demonstration and further optimization of processes. Little access to federal dollars is available in this nutrient area (USDA NRCS, SBIR, etc.)
- *Big Picture*—Ammonia (PM 2.5, health) and nitrates are linked. Mitigating nitrate losses by blowing off ammonia in lagoons/guns makes little sense in larger picture. Similar to tight control of NOx so as to not allow GHG mitigation projects.

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